TABLE I. Experimental argon melting data.

T	D	Molar volume	e (cm³/mole)	A Y7	
Temperature (°K)	Pressure (kilobars)	Fluid	Solid	- ΔV on melting (cm³/mole)	
94.73±0.02	0.451±0.007	27.30±0.02	24.34±0.02	2.96±0.02	
94.74	0.459	27.31			
100.76	0.721	26.89			
108.12	1.051	26.52	24.02	2.50	
110.77	1.186	26.32			
120.85	1.674	25.85	23.65	2.20	
140.88	2.708	24.96	23.04	1.92	
160.40	3.805	24.26	22.54	1.72	
180.15	4.999	23.65	22.08	1.57	
180.20	5.003	23.66	22.11	1.55	
201.32	6.335	23.10	21.69	1.41	

 ± 1 bar at the lower pressures and ± 4 bar at the higher pressures. Construction of this gauge had not been completed at the time the measurements on the solid-fluid phase transition in argon were made, so a Heise Bourdon-tube pressure gauge with somewhat lower sensitivity and accuracy was used in these measurements. The resulting lower accuracy in the determination of the melting pressures will soon be rectified by high-precision measurements of pressure versus temperature along the melting curve for argon and other substances, which are in progress in this laboratory.

The volume of the argon sample was determined by a method not commonly used, but which has several desirable features. In the "normal" data runs the weight of the fluid occupying the entire vessel was measured as a function of pressure and tem-

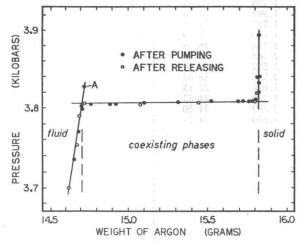


FIG. 4. Isotherm through the solid-fluid phase transition in argon. Point A indicates a pressurization into the supercooled region before the argon began freezing in the vessel.

perature. In addition to these data runs another set of runs was made spanning the same pressure and temperature range, but this time with a solid iron cylinder filling most of the internal volume of the vessel. The difference between the weights of the fluid in the vessel at a given pressure and temperature with and without the iron cylinder in place is just the weight of a volume of the fluid equal to the volume of the iron cylinder at this pressure and temperature. Since this cylinder was subjected only to hydrostatic pressure, the small changes in its volume with pressure and temperature could be calculated accurately from the known equation of state of iron. Such a method for volume determination eliminates the need for assumptions concerning the behavior of a pressure vessel and its closure seals when the vessel is subjected to internal pressure. This is desirable since it was shown, at least for the pressure vessel being used in the present experiment, that the internal volume did not behave according to the usual assumptions.1

PROCEDURE AND RESULTS

Using the apparatus and techniques described above, P-V-T data were obtained for argon (99.995% pure). These data consist of several isotherms, each of which is made up of a number of equilibrium P-V-T points. The procedure for each isotherm, after the system had been initially pressurized, was first to pump a small amount of argon into the vessel or to release a small amount from it. The system was then allowed to equilibrate before the values of the pressure in the system and the temperature and weight of the vessel were recorded. This process was then repeated to obtain a series of points along the isotherm. Immediately after all the points for a particular isotherm

Table II. Experimental P-V-T data for fluid argon (P is in kilobars; V is in cubic centimeters per mole).

210.16°Ka	190.73°	190.73°K		170.36°K		150.73°K	
P V	P	V	P	V	P	V	
0.209 61.45 0.277 51.60 0.360 45.77 0.437 42.71	0.203 0.277 0.348 0.418	51.55 44.99 41.66 39.49	0.209 0.280 0.347 0.422	42.37 39.30 37.50 36.02	0.212 0.274 0.341 0.416	36.79 35.44 34.35 33.38	
0.515 40.43 0.598 38.68	0.483 0.559 0.633	38.02 36.72 35.67	0.489 0.560 0.634	35.00 34.14 33.39	0.489 0.573	32.62 31.91 31.25	
0.782 36.03 0.884 34.98 0.977 34.15 1.072 33.43 1.195 32.61 1.315 31.92	0.729 0.824 0.938	34.56 33.68 32.79	0.719 0.820	32.67 31.93	0.664 0.753 0.854	30.68 30.12	
1.072 33.43 1.195 32.61	1.044 1.174	32.08 31.33	0.930 1.051 1.178	31.23 30.57 29.96	1.112 1.255	29.50 28.96 28.45	
1.552 30.78	1.299 1.432 1.565	30.72 30.14 29.63	1.311 1.458 1.634 1.829	29.42 28.88 28.33	0.755 0.854 0.984 1.112 1.255 1.412 1.575 1.754	27.95 27.50 27.05	
1.939 29.38 2 146 28.75	1.728 1.935 2.136	29.07 28.46 27.93	2.015 2.220	27.78 27.33 26.89	1.958 2.153 2.369 2.605 2.840	26.63 26.25 25.86	
2.355 28.22 2.530 27.81 2.759 27.33 3.035 26.83	2.346 2.552 2.776	27.45 27.03 26.61	2.434 2.648 2.914	26.50 26.10 25.69 25.31	2.605 2.840 3.115	25.48 25.14 24.77	
3.306 26.37 3.577 25.99	3.026 3.261 3.554	26.18 25.83 25.42	3.179 3.450 3.726	24.94 24.62	140.9		
4.123 25.26 4.462 24.88	3.835 4.139 4.478	25.07 24.72 24.37	4.000 4.301	24.31 24.01	P	v	
4.806 24.53 5.143 24.22 5.484 23.95	4.797 5.134 5.486	24.07 23.78 23.50	P 160.4	DEL CARRY DELAN	0.208 0.291 0.380	34.84 33.53 32.47	
5.823 23.67 6.160 23.42 6.464 23.20	5.561 180.21°1	23.43 K	0.203	39.60	0.459 0.537 0.632	31.75 31.14 30.52	
201.29°K	P	V	0.263 0.346 0.409	37.63 35.81 34.79	0.632 0.725 0.823 0.924	29.97 29.48 29.05	
P V	0.203 0.275	46.62 42.05	0.469 0.540	34.01 33.24 32.47	0.924 1.059 1.173	28.53 28.13 27.71	
0.205 57.20 0.275 48.50 0.348 44.12	0.352 0.424 0.487	39.29 37.52 36.39	0.626 0.728 0.833 0.030	31.69 31.02 30.42	1.308 1.445 1.589 1.756 1.939	27.33 26.98 26.58	
0.416 41.55 0.493 39.48 0.554 38.24	0.553 0.634 0.724	35.40 34.45 33.55	0.939 1.053 1.184 1.317 1.454	29.88 29.30 28.82	2 114	26 21 25.88 25.55	
0.624 37.08 0.731 35.69 0.838 34.58	0.831 0.935 1.053	32.67 31.95 31.23	1.454 1.597 1.728	28.37 27.96 27.59	2.310 2.524 2.720	25.22 24.95	
0.941 33.68 1.041 32.95 1.163 32.18	1.160 1.282 1.406	30.67 30.10 29.60	1.940 2.148 2.345	27.09 26.64 26.26	TEA Y		
1.266 31.59 1.401 30.93 1.550 30.28	1.554 1.749 1.949	29.08 28.46 27.92	2.562 2.788 3.041	25.90 25.54 25.18	THA . Y		
1.716 29.66 1.938 28.95 2.355 27.86	2.152 2.355 2.558	27.43 27.00 26.61	3.320 3.582 3.846	24.82 24.50 24.22	1		
2.566 27.40 2.768 27.01 3.002 26.60	2.787 3.038 3.316	26.22 25.81 25.42	5/26	reserve viv	100		
3.249 26.20 3.517 25.80 3.791 25.44	3.573 3.871 4.136	25.09 24.74 24.44					
4.130 25.03 4.458 24.67 4.806 24.33	4.444 4.738 4.916	24.14 23.86 23.71					
5.150 24.03 5.488 23.74 5.824 23.47 6.203 23.20	Standard to our b	na naka ozna naka			2 30 11 2/3W		